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**Study of the interaction of Ni<sup>2+</sup> and Cs<sup>+</sup> on MX-80 bentonite; effect of compaction using the “capillary method”**

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**ABSTRACT**

The goal of the paper is to assess the applicability of sorption models to describe the retention of contaminants on clay materials both in dispersed and compacted states. A batch method is used to characterize the sorption equilibria between Cs, Ni and MX-80 bentonite for solid to liquid ratios varying from 0.5 to 4200 kg/m<sup>3</sup>. For compacted bentonite (dry density of 1100 kg/m<sup>3</sup>), a new method is presented where the material compaction is performed in PEEK capillaries. Sorption edges and isotherms were measured in the presence of a synthetic groundwater. A model considering cation exchange reactions with interlayer cations and surface complexation reactions with edge sites was used for the dispersed state. Montmorillonite was shown to be the dominant interacting phase in MX-80 bentonite. The applicability of the model to compacted bentonite was tested. The results indicate that under conditions where the cation exchange mechanism is dominant, there is no difference between the dispersed and compacted states. For the degree of compaction studied, all exchange sites are available for sorption. For Ni, when surface complexation is the dominant sorption mechanism, a decrease of the K<sub>d</sub> values by a factor of about 3 was observed (pH=7-8, trace concentrations). This could be explained quantitatively by a diminution of the conditional interaction constant between Ni and the edge surface site in the compacted state. One consequence of this decrease is that the contribution of the organic matter content of MX-80 bentonite to the total sorption becomes significative.

## INTRODUCTION

Bentonite is a clay-based natural material which may serve as an engineered barrier in deep geological repositories for radioactive waste (e.g. (1)). The transport of contaminants in water saturated porous clay systems is controlled by sorption (e.g. 2,3). This interaction is typically modelled based on sorption data obtained from batch sorption measurements performed with dispersed bentonite, i.e. on systems with low solid to liquid (S/L) ratios. The literature on sorption of contaminants on dispersed bentonite is voluminous (e.g. (2,3)).

It is necessary to assure that sorption parameters obtained on dispersed materials are able to describe the sorption processes in compacted media. This appears notably necessary for high degrees of compaction where the notion of free water is not anymore valid (4) (i.e. for a dry density above  $1700 \text{ kg/m}^3$ ). The experimental retention data in the compacted state (for dry densities varying between 400 to about  $1800 \text{ kg/m}^3$ ) are generally determined indirectly, i.e. from migration studies (3,5, 6, 7, 8). The comparison with the results obtained with dispersed bentonite shows that material consolidation has in some cases no effect on retention, in other cases it has a positive (increase of the retention) or negative (decrease of the retention) effect (3, 5, 6, 7, 8,9,10). The origin of the effect appears unclear; either the transport or the retention model is criticized (2-7,9,10). Concerning the retention model, site accessibility is advanced as an explanation (9).

To better understand the relation between the retention of contaminants in dispersed and compacted systems, it appears fundamental to develop new methodologies to measure sorption data directly on compacted materials (9).

In this paper, a batch method allowing the characterization of the sorption equilibria between the contaminants and bentonite for high solid/liquid ratios is presented. The consolidation has been realized within capillaries. The low mass of bentonite used in the capillary allows to change easily the experimental conditions. The method is applied to Cs and Ni with MX-80

bentonite for a S/L ratio of 4200 kg/m<sup>3</sup>. pH edges and isotherms measured in the presence of a synthetic groundwater are compared with those measured in the dispersed state (S/L=0.5-10 kg/m<sup>3</sup>). The results were modeled based on published models obtained with pure clay materials (11,12,13). The effect of secondary phases on the total retention was discussed.

## **MATERIAL AND METHODS**

### **(A) Materials**

All chemicals used were of analytical purity. MX-80 bentonite was used without any purification, except for some sorption tests realized with Ni in the dispersed state, where bentonite was treated with H<sub>2</sub>O<sub>2</sub> (S/L=10 kg/m<sup>3</sup>; NaCl 0.05M; H<sub>2</sub>O<sub>2</sub> 12%, T=70°C; five treatments) to selectively remove organic matter (14). The montmorillonite fraction amounts to 84% (11). Natural Ni and Cs were found in MX-80 bentonite with amounts of 5.4mg/kg and 0.11mg/kg, respectively (15). Experiments performed under acidic conditions (pH=2.5, NaNO<sub>3</sub> 0.05M) showed that about 65% of the inventories of Cs and Ni were mobilizable (15). A water content of 8% was determined by drying at 105°C for 12 hours and taken into account for the calculation of the bentonite concentration in the dispersed state. HTO, <sup>63</sup>Ni and <sup>137</sup>Cs (with carrier) were obtained from CERCA - FRAMATOME, AMERSHAM and CEA/DAMRI, respectively. Capillaries in PEEK of 1 mm internal diameter were used for the experiments realized with compacted bentonite.

### **(B) Sorption study**

All experiments were performed at T=23±3°C. Sorption data were measured using a typical water composition of the claystone of the Bure site (see Table 1). Two types of data sets were collected: in the first case, sorption is studied at initial fixed metal ion concentration as a function of pH (sorption pH edges) and in the second case, sorption was measured as a

function of metal ion concentration at constant pH (sorption isotherms). For the measurement of pH edges, the pH value was varied between 4 and 9 using NaOH and HClO<sub>4</sub> stock solutions. For fixing the pH above a value of 4 for sorption studies, MES (2-(N-Morpholino)ethane-sulphonic acid), MOPS (3-(N-Morpholino)propane-sulphonic acid) and/or TRIS (Tris(hydroxymethyl)aminomethane) buffers at a concentration of 2.10<sup>-3</sup>M were used. They are known to not alter the sorption behaviour of metal ions on clay materials in the dispersed state (12). Some complementary experiments without buffers were performed for Ni to confirm the non-affect in the compacted state. It was checked (in both consolidated and dispersed states) by comparison to data measured without buffers that MES, MOPS and TRIS reagents did not alter the sorption behaviour of Ni and Cs. The initial concentrations of Ni and Cs introduced in the system were always sufficiently high allowing to neglect the content of Cs and Ni naturally present in bentonite: the added metal ions concentrations were higher than 90 and 99% of the natural content for Ni and Cs, respectively. Experiments were performed either in air atmosphere or in an inert gas glove box (N<sub>2</sub>). In air atmosphere, the pH range studied was limited to values below 7.8 to avoid any precipitation of carbonate phases of Ca and Mg. The results showed no significant differences when CO<sub>2</sub> is present or not; this indicates that carbonates have not a significant influence in the experimental conditions of this study. Therefore, no distinction was made in the figures between the experiments performed in the presence or absence of CO<sub>2</sub>.

**Compacted state.** A scheme of the methodology is given in Figure 1. To control the pH value of the bentonite porewater, a pre-equilibration of the aqueous and solid phases was necessary. This was done in the dispersed state (S/L=10 kg/m<sup>3</sup>). After stabilization of the pH value (it varies not more than 0.05 pH unit for one day), the solution was removed and replaced by a fresh one. The procedure was repeated till the equilibrium conditions were reached. Then, the

solid and liquid phases were separated at 0.2  $\mu\text{m}$ , the solid was dried at 35°C, crushed and sieved at 63  $\mu\text{m}$ .

The consolidation of the pre-equilibrated bentonite was realized in PEEK capillaries of about 3 mm in length with 1 mm internal diameter. A small amount of bentonite was introduced in the capillary at one extremity while the other was blocked. The bentonite was then compacted manually using a 1 mm-diameter steel drill. This step was repeated till the capillary contained about 3-4 mg of bentonite. No filter was used at the interface between the water and the compacted material. The capillaries thus prepared were put into the corresponding external solution (3 mL) for pore saturation. After swelling, the capacity of the capillaries to compact bentonite was estimated to be equal to  $(776\pm 106)$  mm (filling height in the capillary) per gram of saturated bentonite. Then, after a contact time of at least 3 days, three types of experiments were conducted in parallel:

1/ The goal of the first series of experiments was to define in the compacted state the liquid and solid phases for the determination of the solid to liquid ratio, S/L. In this study, the liquid phase, or the pore water refers to the free water, i.e. the water not bound to bentonite. This pore water volume ( $\theta_p$ ) was probed using Tc(VII) and I(-I) (16). It was determined only at pH=7.8 for high concentrations ( $10^{-5}$ - $10^{-4}$  M of Tc(VII) and  $10^{-3}$  M of I(-I)) where the adsorption of the anions can be neglected. The pore volume, composed of the bound+free water, is determined using HTO tracer ( $\theta_{\text{HTO}}$ ). It was additionally assessed by drying saturated and compacted bentonite at 105°C ( $\theta_{105}$ ).  $\theta_{\text{HTO}}$  and  $\theta_{105}$  were determined for all pH values. The porosity was defined in this work by the volume of porewater (in  $10^{-3}$  m<sup>3</sup>) per kilogram of dry MX-80 bentonite. The mass of dry bentonite referred to the mass without the bound water, i.e. the S/L ratio corresponds to  $\theta_{\text{HTO}}^{-1} 10^3 \text{ kg/m}^3$ .

2/ The second series gives the equilibrium state of the system when the sorption equilibrium (between the contaminant and compacted bentonite) is reached. It is characterized by the pH

value and the composition of major (Na, K, Mg, Ca) and minor (Al, Si, Fe) ions in the external solution.

3/ The third series implies the measure of the sorption data either at equilibrium or as function of the contact time (between the compacted material and the solution). After a contact time of x days, the saturated bentonite in the capillaries was pushed out, the first part of the compacted material was removed (about 0.3mm in height) and the material was weighted ( $m_{tot}$ ). Then, it was dried at 105°C (determination of  $\theta_{105}$ ) or mixed with 0.1M HCl at a solid to solid ratio of 1 kg/ m<sup>3</sup> for analysis of the total activity in the solid ( $A_{tot}$ ; determination of  $\theta_p$ ,  $\theta_{HTO}$  and sorption data). The activity in the external solution was also measured ( $A_f$ ).

The activity in the porewater in Bq for a given sample is:

$$A_p = \frac{m_{tot} \cdot \theta_p \cdot A_f}{(1 + \rho_{H2O} \theta_{HTO})} \quad (1)$$

with  $m_{tot}$  in kg and  $A_f$  in Bq/L. The volumic mass of water ( $\rho_{H2O}$ ) is supposed to be equal to 1 10<sup>3</sup> kg/m<sup>3</sup>.

For the experiments conducted with Tc(VII) and I(-I),  $A_p = A_{tot}$ . For the sorbed elements, the  $K_d$  value (in 10<sup>-3</sup> m<sup>3</sup>/kg) can be derived according to the following relation:

$$K_d(C) = \frac{A_{tot} - A_p}{A_p} \cdot \theta_p \quad (2)$$

with  $A_{tot}$  in Bq.

For each  $K_d$  value, at least three experiments were performed. The Figures give the average values together with the standard deviations.

**Dispersed state.** All experiments were conducted in polyethylene tubes for S/L ratios varying from 0.5 to 10 kg/m<sup>3</sup>. A pre-equilibration of the system was performed according to the methodology presented for the compacted state. Then, the element and the corresponding

tracer were introduced in the suspension at the desired concentration. The suspensions were stirred for 7 days to reach equilibrium. Studying the sorption kinetics, this time was found to be sufficient to reach equilibrium. The solid phase was separated from the aqueous one by centrifugation for 30 minutes at 11000 g. Aliquots of the supernatant were analysed to derive the distribution coefficients using the following expression:

$$K_d(D) = \frac{A_{\text{tot}} - A_L}{A_L} \cdot \frac{L}{S} \quad (3)$$

where  $A_{\text{tot}}$  is the total activity added to the system (Bq),  $A_L$  is the equilibrium activity in the liquid phase (Bq), and  $S/L$  the solid to liquid ratio in  $10^3 \text{kg/ m}^3$ .

**(C) Analytical Methods.** A PQ-Excel ICP-MS (VG-Elemental) was used to analyse the major and minor cations (see Table 1). HTO, Cs ( $^{137}\text{Cs}$ ) and Ni ( $^{63}\text{Ni}$ ) analysis were performed by liquid scintillation counting using a Packard 2550 TR/AB Liquid Scintillation analyzer. The scintillation cocktail was ULTIMA GOLD AB<sup>TM</sup> (Packard).

#### **(D) Modelling**

The objective is to use the data measured in the dispersed state to define an operational model allowing to predict the retention in the compacted state. The basic assumption in both cases is that Cs and Ni sorb predominantly on the montmorillonite fraction of MX-80 bentonite.

The minerals dissolution is considered indirectly by introducing the measured concentration of Si, Al and Fe in the solution (Table 1). At the solid/water equilibrium, the composition of the exchange sites as well as the speciation of the surface sites are calculated for the solution composition (Table 1) using the parameters given in Table 2.

The acid-base properties of edge sites is still a matter of discussion in the literature (17). In the present study, the simplified two-pK nonelectrostatic model from Bradbury et al. (13) is used. Although it has not a real physical meaning (18), it remains an “operational” model



tested with a lot of radionuclides (see references quoted). In the model, the electrostatic term is not explicitly represented. Either it is of significance importance and the pH-dependent coulombic contribution is included in the interaction constants (19) or it can be ignored (18)

For compacted and dispersed states, sorption is described by pH-dependent interaction with clay edges and by the cation exchange in the interlayer and on the basal plane surfaces. The parameters used to describe the interaction between Ni and Cs and montmorillonite are included in Table 2. Except for the major element exchange, the competition of metallic impurities with Cs and Ni for sorption sites is not considered. First, the amount of mobilized metallic impurities from MX-80 bentonite is not higher than  $10^{-7}$  mol/g (15). Second, the pre-equilibrium step following the batch procedure (Figure 1) is expected to reduce impurities to even lower values. Third, considering the S/L ratios explored in the present study, the number of sorption sites is much higher than the concentration of impurities.

The Phreeqc code was used to model the sorption results using the Llnl.dat database to calculate the speciation in aqueous solution (20). For the kinetic experiments, the sorption model was coupled with a transport model considering a diffusion process. For the transport part, the only fitting parameter was the diffusion coefficient.

## **RESULTS AND DISCUSSION**

### **(A) System characterization**

**Porosity characterization in the compacted state.**  $\theta_{\text{HTO}}$  and  $\theta_{105}$  were found similar irrespective of the pH value. The pore volume determined by drying at 105°C amounts to  $(0.41 \pm 0.05) 10^{-3} \text{ m}^3/\text{kg}$ . This value appears slightly lower than that determined with HTO  $(0.49 \pm 0.03) 10^{-3} \text{ m}^3/\text{kg}$ . The dry density of bentonite amounts to  $1100 \pm 60 \text{ kg/m}^3$ .

The free pore water volume probed by  $\text{TcO}_4^-$  and  $\text{I}^-$  was found to be equal to  $(0.24 \pm 0.04) \cdot 10^{-3} \text{ m}^3/\text{kg}$  independent on the concentration and choice of the anion. Due to the anionic exclusion phenomenon, the anions access neither to the water in the double layers associated with external surfaces of the clay stacks, nor in the interlayer space (16). The distribution free / bound water appears therefore in the proportions 49:51%. Considering a value of 0.3 nm for one water layer, the different specific surface areas of montmorillonite (i.e. 30 and 8.5  $\text{m}^2/\text{g}$  for the external basal and edge surfaces, respectively and 750  $\text{m}^2/\text{g}$  for the interlayer surface area) (18) and 2-2.5 (21) and 2-3 (21-22) water layers for the external and internal surfaces, respectively, one would calculate a free porosity value of  $\theta_p = 0.18 \pm 0.06 \text{ L/kg}$ . The prediction appears coherent, at least within experimental errors, with the experience.

The S/L ratio corresponding to  $\theta_p^{-1}$  amounts to 4200  $\text{kg}/\text{m}^3$ . This value is supposed to be constant in the pH range investigated (4-9).

**Water/solid Equilibrium.** Table 1 summarises the characteristics of the solution (pH, major and minor concentrations) after reaching sorption equilibrium for dispersed and consolidated states. A slight increase in the ionic strength is observed in the compacted state. This may be explained by a slight evaporation of the external solution after the equilibrium period. For the minor elements, the concentration remains nearly constant, irrespectively of the system considered. The measured concentrations are similar to values measured for equilibrium of purified montmorillonite with water (12,17).

## **(B) Sorption studies**

**Dispersed state.** Experimental results for Cs and Ni are given in Figures 2. Model parameters describing the interaction of Cs and Ni with montmorillonite are already available in the literature. The works of Bradbury & Baeyens (for Ni) (12,13) and Hurel et al. (for Cs) (11)

performed under well-controlled conditions (simplified medium, purified Na-montmorillonite) with Swy-1 and MX-80 Na-montmorillonite, respectively, were chosen as references for this study. For Cs, the lines in Figure 2 correspond to the calculation made considering an interaction governed by the exchange sites using only the published exchange constant (11). The prediction agrees to the experimental data for equilibrium solution concentrations ( $C_L$ ) above  $10^{-6}$  M. At lower concentration, the prediction underestimates the sorption by a factor of about 0.6. This indicates the existence of a second interacting site governing Cs sorption for trace concentrations. According to the literature, this may be explained by the interaction of Cs with edge sites (11,23). However, the pH-edge measured for trace concentrations (Fig. 2B) shows that the interaction is not affected by the change in pH. The mechanism associated to this second site must also be a cation exchange mechanism with interlayer cations. This could be the result of different binding energies of Cs in the interlayer due to different substitutions in octahedral and tetrahedral sites. It may alternatively as well be due to the existence of another clay mineral, in low amount, in MX-80 bentonite. Under a quantitative point of view, the interaction of Cs with this new exchange site must be stronger than that presented by montmorillonite (i.e.  $\equiv X$  site, Table 2). The new site (i.e.  $\equiv X_a$  site, Table 2) is introduced in the model with the parameters given in Table 2. It shall be noted that the parameters are applicable only for the conditions of the present study.

The sorption edge data and isotherms obtained for Ni are presented in Figures 2C-D together with the published sorption edge data obtained with (MX-80) Na-montmorillonite in  $\text{NaNO}_3$  0.05 M (15) (Figure 2C). The latter series is used to test the model of Bradbury & Baeyens obtained for montmorillonite extracted from Swy-1 bentonite (13). As shown by the dashed line in Figure 2C, the model over-estimates the retention by more than one order of magnitude when the surface complexation mechanism dominates ( $\text{pH} > 5$ , trace concentrations). This deviation can be explained with the parameters of Bradbury & Baeyens considering the

presence of a strong competing agent, like Zn, at a concentration of  $10^{-5}$  M. Such a concentration was not detected and a competition effect is therefore not expected. The agreement becomes better if the interaction of Ni with the strong site is entirely neglected. This modified model allows as well to describe the data measured with bentonite and the synthetic groundwater (SGW) (solid lines in Figures 2C and 2D). The results may indicate that the strong site present on montmorillonite extracted from Swy-1 bentonite (“Swy-1 montmorillonite”) is not present on the clay material extracted from MX-80 bentonite (“MX-80 montmorillonite”).

A detail examination of the data reveals however a slight disagreement between the model and the experience. In the pH range between 4 and 6, for trace concentrations, the model underestimates the retention. This may be explained by a pH-dependent interaction of Ni with another site. An estimation of the parameters associated to this interaction were obtained as follows: the apparent deprotonation constant ( $k_a$ ) was fixed while the number of sites and the interaction constant were fitted using the isotherm measured at pH=5.8 (Figure 2F). The pH-edge for trace concentration was then calculated and compared with the experimental data (Figure 2E). This was done for log  $k_a$  values varying from -8 to -4 (see Figure 2E). The best agreement is found with the parameters given in Table 2. The pKa value appears lower than those generally found for mineral surface sites. MX-80 bentonite contains about 0.4% in weight in organic matter (24). Organic matter, and particularly carboxylate groups, could be responsible for this interaction. This assumption is confirmed by the data measured with bentonite treated with  $H_2O_2$ : between pH=4 and pH=7, the calculation made with the modified model of Bradbury & Baeyens (13) agrees with the experiment without considering the interaction of Ni with a secondary phase (Figure 2C, gray symbols).

In conclusion, the cationic exchange mechanism dominates the sorption for Ni concentrations above  $10^{-4}$ M and pH<4. Organic matter is the dominant interacting phase for trace

concentrations and pH values varying from 4 to 6. Finally, in conditions relevant to nuclear waste disposal (pH>7, trace concentrations) (25), the sorption is governed by a surface complexation mechanism with edge surface sites. Montmorillonite appears in this case to be the dominant interacting phase.

### **Compacted state**

*Kinetic.* The design can be decomposed into two systems: the external solution in equilibrium with the atmosphere and the compacted medium where the porewater is locally in equilibrium with bentonite for a high solid to liquid ratio. Before the addition of Cs or Ni, and according to the methodology given in Figure 1, the whole system is considered in equilibrium, i.e. the water of the external solution (in equilibrium with the atmosphere) has the same composition as the free pore water. In the presence of Cs or Ni, the equilibrium is disturbed by the sorption of the element on bentonite. Two processes need to be considered:

- The diffusion of Cs or Ni from the external solution to the porewater and the sorption of the element on bentonite.
- The re-equilibration of the pore water composition with respect to the water of the external solution after the sorption reaction.

In the conditions of the study, the volume of the external solution is much higher than the volume of the porewater ( $V(\text{external solution})/V(\text{porewater}) > 2.10^6$ ). Therefore, the composition of the external solution does not vary during the sorption process. The equilibration process was followed by analysing the temporal evolution of the content of Ni or Cs in the compacted system (i.e. pore volume + bentonite). The sorption equilibrium is considered to be reached when it does not vary anymore with contact time.

This is illustrated in Figure 3 for Ni and Cs. The amount of Ni and Cs in the capillaries increases as the contact time increases till a plateau is reached after about 40 days for both

cations. The gray zones correspond to the simulation made with the PHEEQC code. The calculation takes the variation of the mass of saturated bentonite in the different capillaries ( $m_{\text{tot}}=3.9\pm 0.5$  and  $4.0\pm 1.0$  for Cs and Ni, respectively) and the uncertainty associated to the consolidation capacity of the capillaries ( $776\pm 106$  mm per gram of saturated bentonite) into account. The increase in concentration is well described by a diffusion process of Ni, Cs from the external solution to the compacted clay medium with an effective diffusion coefficient of  $5.10^{-10}$  m<sup>2</sup>/s for both cations. At equilibrium, in the case of Ni, a decrease of the retention capacity of bentonite, as compared to that determined in the dispersed state, is needed for a good agreement (see next part).

Based on these results, equilibration times were fixed to 2 and 3 months for Cs and Ni, respectively.

*Data at equilibrium.* The experimental data measured for Cs with the compacted material are given in Figures 4A-B together with the data measured in the dispersed state. A good agreement is found between both series of experiments. As indicated by the solid lines, the model derived from the dispersed state describes as well the data in the compacted state. The cation exchange capacity and the constants characterizing the interaction appear therefore not significantly affected by the consolidation.

Sorption edges and sorption isotherms obtained for Ni in the compacted state are displayed in Figures 4C-F. The results obtained in the presence and absence of buffers are nearly identical. As it is the case in the dispersed state (12), the buffers used in (12) do not alter the sorption behaviour of Ni on compacted bentonite. When the cation exchange mechanism (Figures 4C and 4D) and/or the interaction of Ni with organic surface sites (Figure 4E) dominates, the agreement between dispersed and consolidated states is good.

On the other hand, when the surface complexation mechanism with edge sites dominates, a significant deviation between model and experiment is observed (Figure 4F). Quantitatively,

this may be explained by a modification of the interaction constant or by a diminution of the number of sites. Both assumptions were tested in Figure 5 and the results show that the first assumption is more reliable. An interesting consequence of this decrease is that even if the clay part of MX-80 bentonite remains the predominant interacting phase, organic matter, in spite of its low content, becomes a significant interacting phase in the compacted system in conditions relevant to nuclear waste disposal (it contributes to about 20% of the total sorption capacity of bentonite). The origin of the decrease appears unclear. It may be explained either by a modification of the complexed species in the compacted species (a change of the intrinsic binding constant) or by a modification of the electrostatic term contribution in the conditional constant. The origin of the effect could arise from the interaction between edge surfaces in the compacted state (26). However, further experiments are necessary to understand the exact nature of the consolidation effect on the retention.

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**Table 1. Analysis of the equilibrium conditions.**

State	pH*	MAJOR CATIONS				MINOR IONS		
		[K]	[Ca]	[Na]	[Mg]	[Si]	[Al]	[Fe]
		In mM				In $\mu$ M		
Consolidated state	4 - 9	0.6 $\pm$ 0.2	6.6 $\pm$ 1.1	57 $\pm$ 20	4.4 $\pm$ 0.7	107 $\pm$ 43	0.28 $\pm$ 31	<0.9
Dispersed state	4 - 9	0.4 $\pm$ 0.1	5.9 $\pm$ 0.4	37 $\pm$ 8	3.0 $\pm$ 0.7			

\* for pH>7.8, experiments are performed in an inert atmosphere

**Table 2:** modelling parameters

<b>Bentonite description</b>					
<b>Site types</b>		<b>Site capacities *</b>		<b>[REF]</b>	
Exchangeable interlayer cations $\equiv X$		64 meq/100g		(11)	
Exchangeable interlayer cations $\equiv X_a$		2.10 <sup>-3</sup> meq/100g		this work <sup>†</sup>	
Edge site $\equiv S^{1s}OH$		1.7 μmol/g		(13,18)	
Edge site $\equiv S^{1w}OH$		33.6 μmol/g		this work	
Edge site $\equiv S^2OH$		33.6 μmol/g			
Site $\equiv S-OH^{**}$		0.11 μmol/g			
<b>Water / solid equilibrium</b>					
<b>Reaction</b>	<b>logK<sub>int</sub> (this work)</b>		<b>LogK<sub>int</sub> (reference study)</b>		
	<b>Dispersed bentonite</b>	<b>Compacted bentonite</b>			
$\equiv S^{1w(s)}OH \rightleftharpoons \equiv S^{1w(s)}O^- + H^+$	-7.9		-7.9	(13)	
$\equiv S^{1w(s)}OH + H^+ \rightleftharpoons \equiv S^{1w(s)}OH_2^+$	4.5		4.5		
$\equiv S^2OH \rightleftharpoons \equiv S^2O^- + H^+$	-10.5		-10.5		
$\equiv S^2OH + H^+ \rightleftharpoons \equiv S^2OH_2^+$	6		6		
$\equiv SOH \rightleftharpoons \equiv SO^- + H^+$	-4.7		-	This work	
$K^+ + \equiv X(a)Na \rightleftharpoons \equiv X(a)K + Na^+$	0.6		0.6	(27)	
$Mg^{2+} + 2 \equiv X(a)Na \rightleftharpoons \equiv X(a)_2Mg + 2Na^+$	0.34		0.34		
$H^+ + \equiv X(a)Na \rightleftharpoons \equiv X(a)H + Na^+$	0		0	(18)	
$Ca^{2+} + 2 \equiv X(a)Na \rightleftharpoons \equiv X(a)_2Ca + 2Na^+$	0.4		0.4		
$CaCl^+ + \equiv X(a)Na \rightleftharpoons \equiv X(a)CaCl + Na^+$	2.5		2.5		
$CaOH^+ + \equiv X(a)Na \rightleftharpoons \equiv X(a)CaOH + Na^+$	2.5		2.5		
<b>Sorption reactions</b>					
<b>Element</b>	<b>Reaction</b>	<b>logK<sub>int</sub> (this work)</b>		<b>LogK<sub>int</sub> (reference study)</b>	
		<b>Dispersed bentonite</b>	<b>Compacted bentonite</b>		
Cs	$Cs^+ + NaX \rightleftharpoons CsX + Na^+$	1.65		1.65	(11)
	$Cs^+ + NaX_a \rightleftharpoons CsX_a + Na^+$	6		-	This work
Ni	$Ni^{2+} + 2NaX \rightleftharpoons NiX_2 + 2Na^+$	0.49		0.49	(13)
	$Ni^{2+} + \equiv S^{1w}OH \rightleftharpoons \equiv S^{1w}ONi^+ + H^+$	-3.1	-3.6	-3.1	
	$Ni^{2+} + \equiv S^{1s}OH \rightleftharpoons \equiv S^{1s}ONi^+ + H^+$	n.c.		-0.1	
	$Ni^{2+} + \equiv SOH \rightleftharpoons \equiv SONi^+ + H^+$	1.3		-	This work

Legend: \* clay content of 84% (11); \*\* site considered only for Ni; n.c.: not considered; † site considered only for Cs.  $\equiv S^{1w(s)}OH$  means  $\equiv S^{1w}OH$  or  $\equiv S^{1s}OH$  surface sites.  $\equiv X(a)$  means  $\equiv X$  or  $\equiv X_a$  exchange sites.

## Figure captions

**Figure 1 :** Description of the procedure followed to measure the retention data in the compacted state.

**Figure 2 :** Sorption of Cs (A,B) and Ni (C-F) on bentonite in the dispersed state. Sorption isotherm (A) and sorption edge (B) measured for Cs. The calculation is made with (solid line) or without (dashed line) considering the exchangeable interlayer cations  $\equiv Xa$  (see Table 2). Sorption edges (C,E) and sorption isotherms (D,F) measured for Ni. (O) Data obtained in simplified conditions (15); (○) data measured with MX-80 bentonite treated with  $H_2O_2$ . The calculation in Figures C and D is based on the model of Bradbury & Baeyens (13) with (dashed line) or without (solid lines) the strong site (see Table 2). For Figures E, F, the site  $\equiv S-OH$  is considered (see Table 2 and text).

**Figure 3:** Sorption kinetics of Ni (●) and Cs (O) on compacted bentonite. Cs:  $C_{tot} < 5.10^{-9}$  M; pH=7.8 ; Ni :  $C_{tot} = 5.10^{-8}$  M; pH=7.8. The gray zones correspond to the simulation made with the PHEEQC transport code considering a diffusive transport (see text).

**Figure 4 :** Comparison between dispersed and consolidated states for Cs (A,B) and Ni (C-F). Sorption isotherm (A) and sorption edge (B) measured for Cs. Sorption isotherms at pH=4.2 (C) and 5.8 (E) and sorption edges for  $C_{tot(L)} = 1.10^{-3}$  M (D) and  $1.10^{-7}$  M (F) measured for Ni in the compacted (solid points) and dispersed (open points) states. The solid lines correspond to the prediction made with the model obtained for dispersed bentonite (see Table 2).

**Figure 5:** Sorption isotherm (A) (pH=7.8) and sorption edges (B) ( $C_L = 1.10^{-7}$  M) measured for Ni in the compacted state. The lines correspond to model adapted to the compacted medium considering either a diminution of the interaction constant (solid line,  $\log K = -3.6$ ) or a diminution of the number of sites (dashed line,  $0.046 \mu\text{mol/g}$ ).

Figure 1

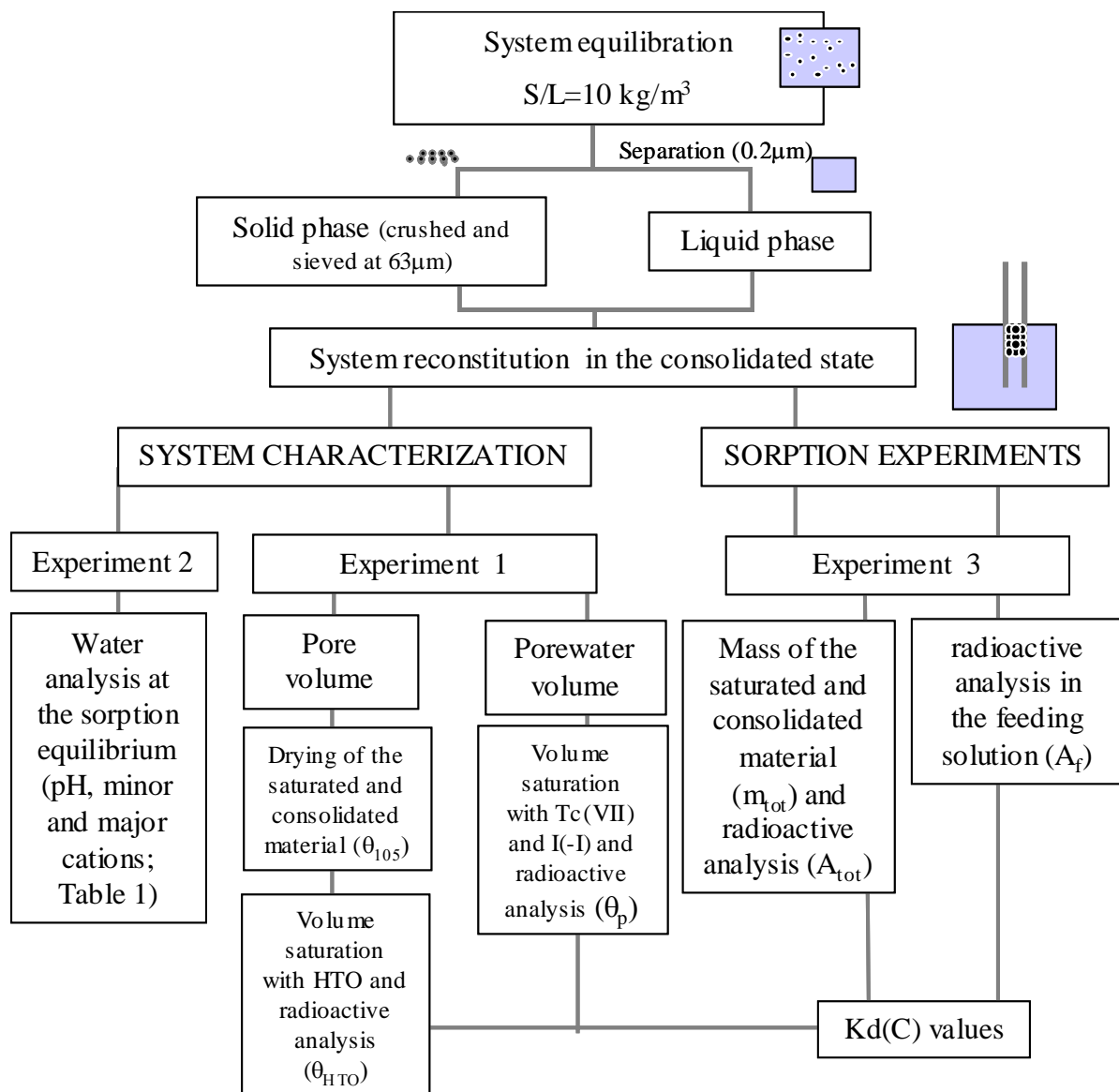


Figure 2

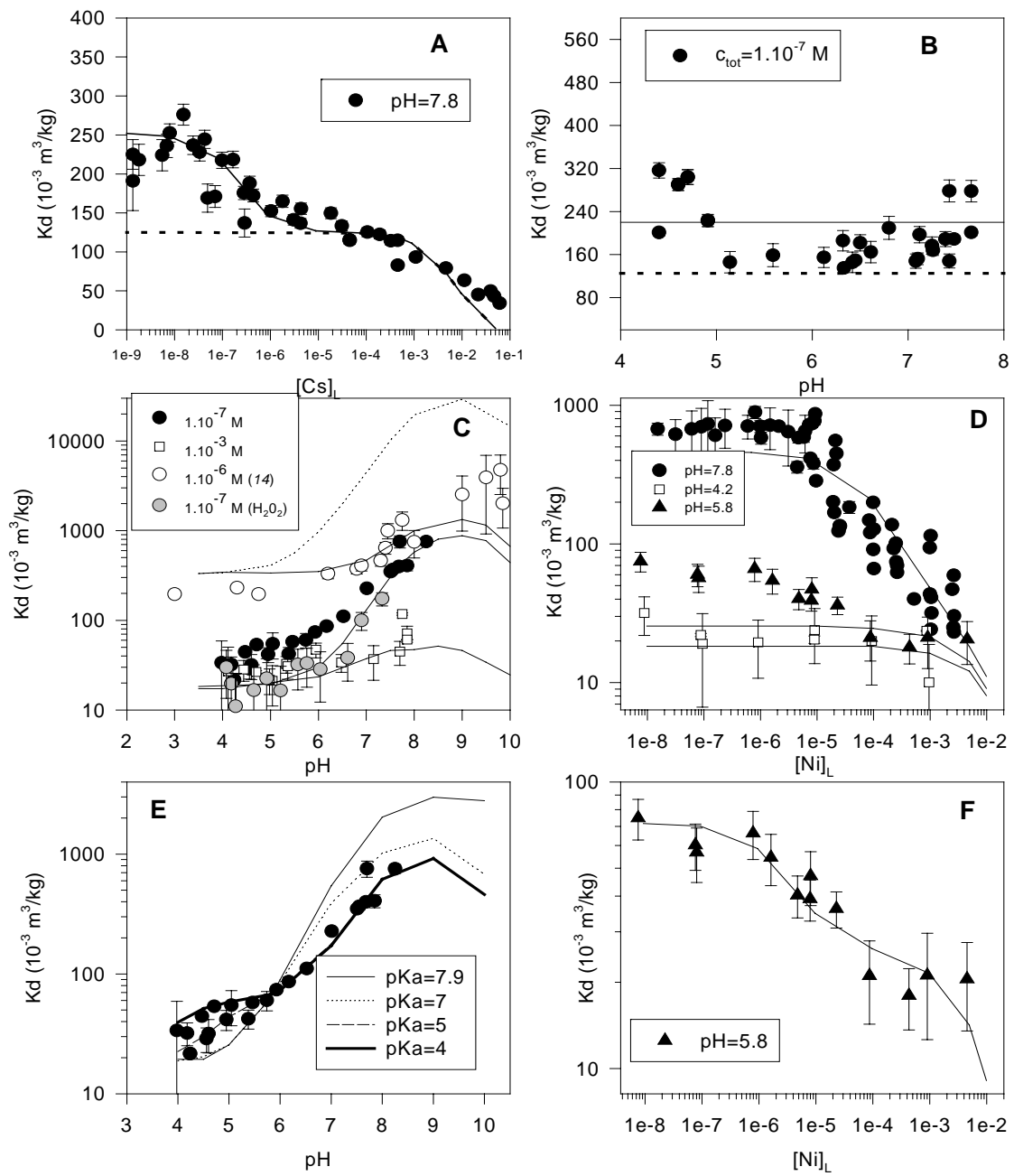




Figure 3

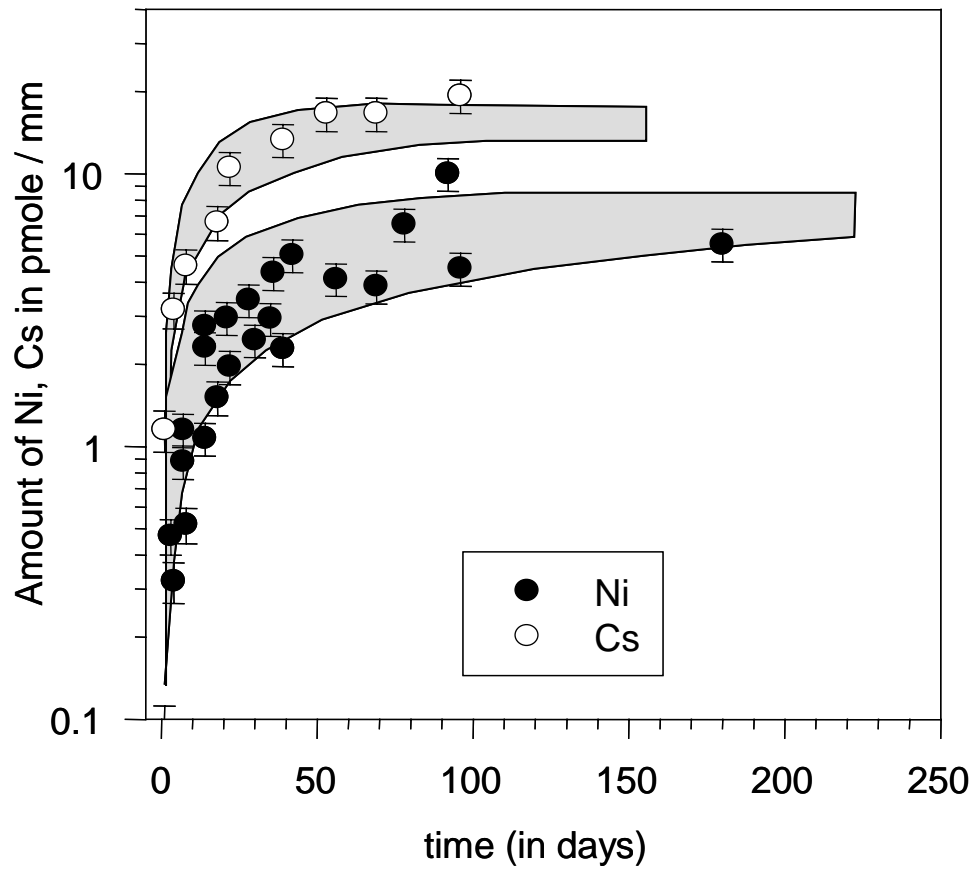


Figure 4

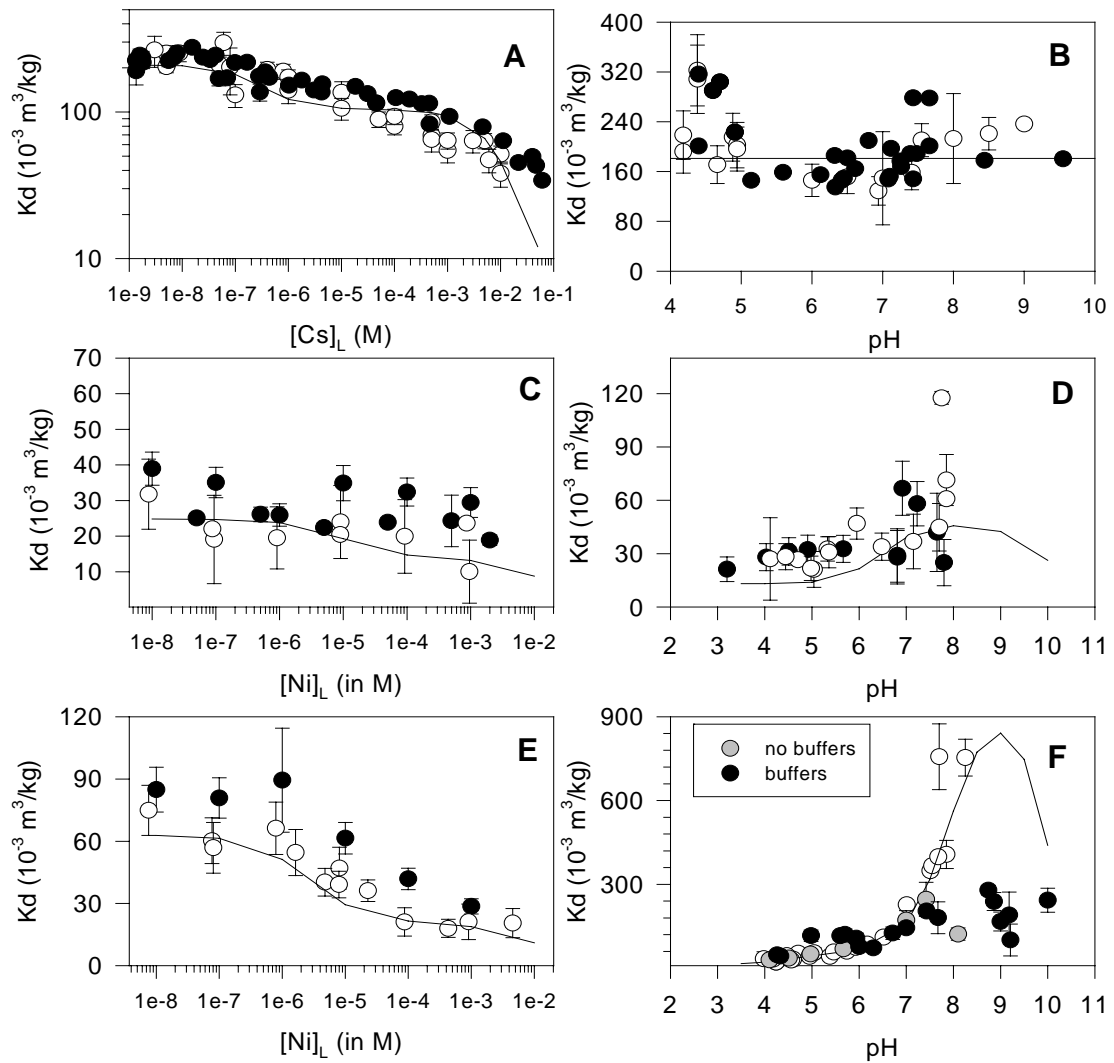


Figure 5

